

High Temperature (Industrial) Heat Pumps: An Untapped US Industrial Process Energy Efficiency Opportunity

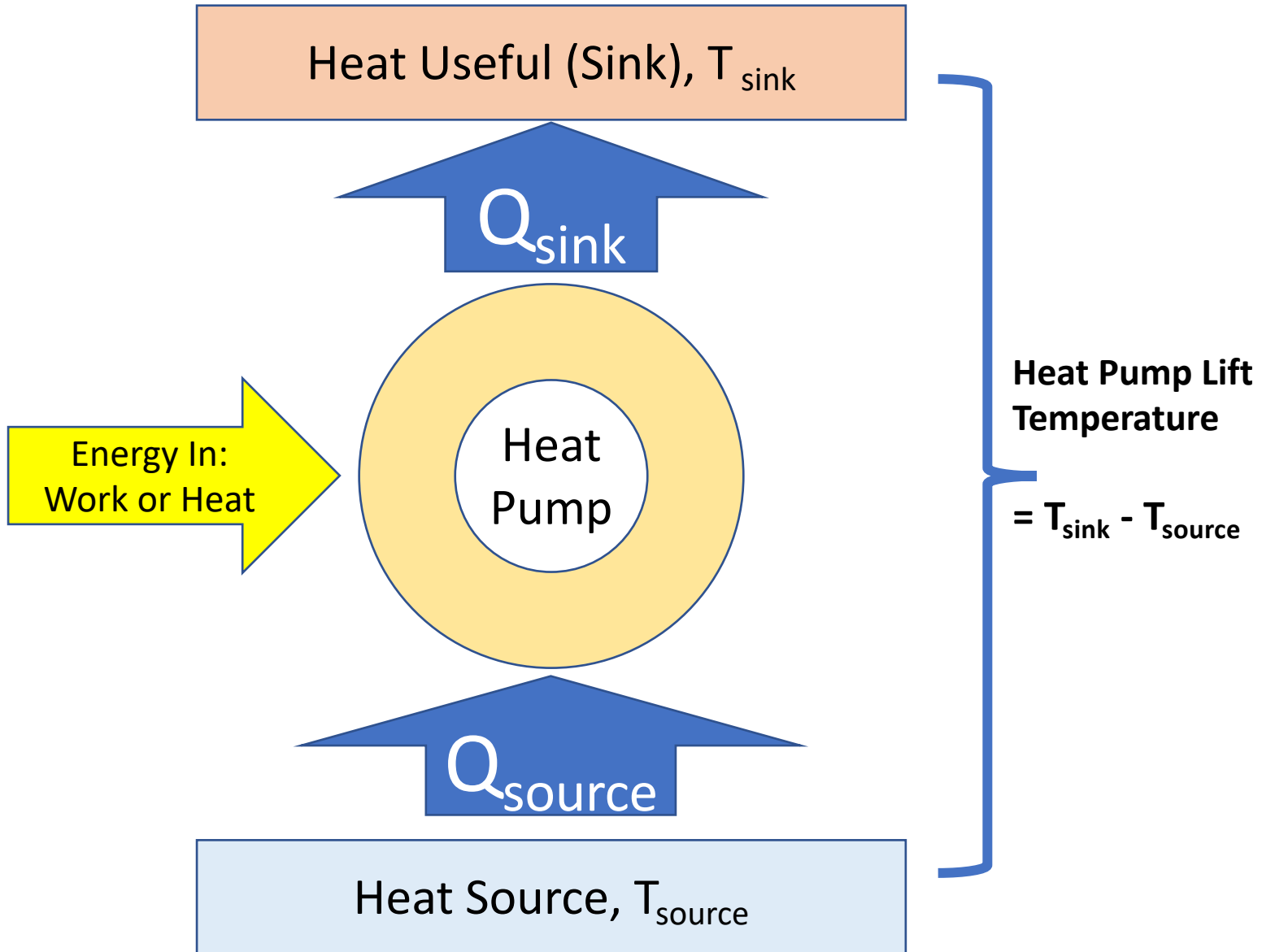
Paul Scheihing, 50001 Strategies

In collaboration with Neal Elliott and Ed Rightor, ACEEE

Low Temperature Industrial Processes Workshop

February 3, 2021

Fundamentals of Heat Pumps



$$\text{COP}_{\text{heating}} = Q_{\text{sink}} / \text{Energy In}$$

$$\text{COP}_{\text{carnot, heating}} = T_{\text{sink}} / (T_{\text{sink}} - T_{\text{source}})$$

$$\text{COP}_{\text{heating}} = \text{Carnot Eff.} * \text{COP}_{\text{carnot, heating}}$$

Heat pump Carnot Eff.
ranges from ~30 - 60%

***Less lift temperature equals
greater heat pump efficiency***

Typical HTHP heat sources and sinks

Space Heating
30 C to 70 C

Drying Process
100 C to 250 C

Process Heat

Steam
100 C to 220 C

Hot water
50 C to 120 C

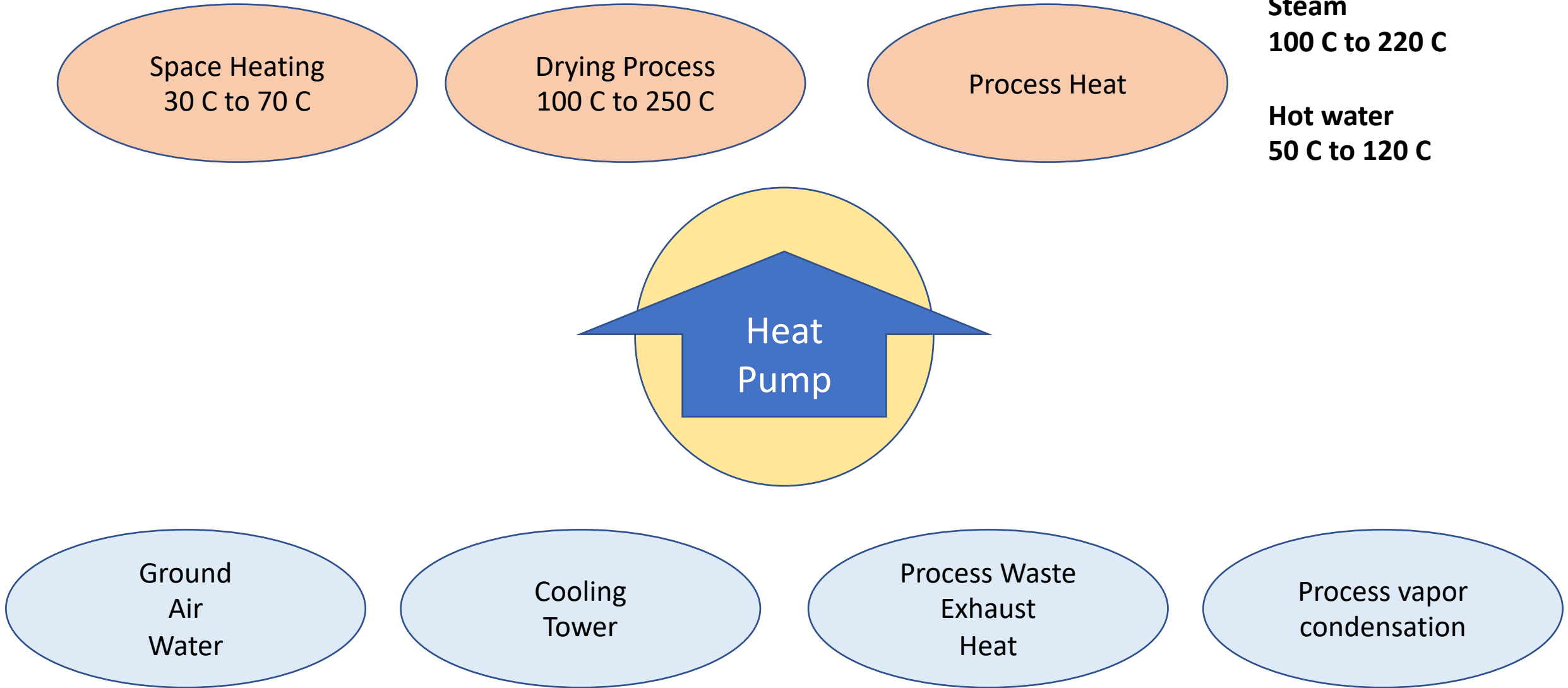
Heat
Pump

Ground
Air
Water

Cooling
Tower

Process Waste
Exhaust
Heat

Process vapor
condensation



US DOE Heat Pump Program & IEA Annex 21 Study

IEA Annex 21 Study (1993 – 1995)

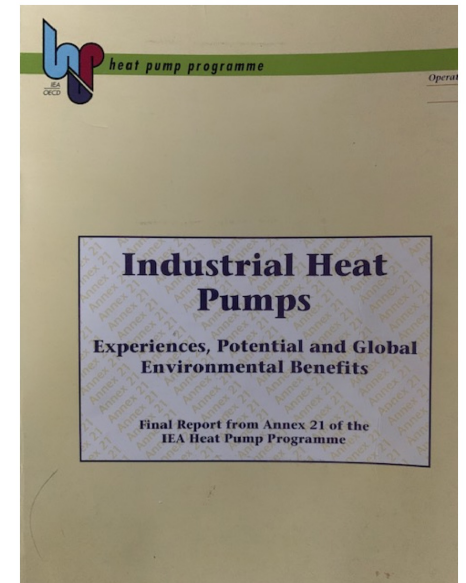
- Industrial Heat Pumps: Experiences, Potential and Global Environmental Benefits

- 8 countries collaborated
- 35 processes evaluated for IHP potential across all 8 countries
- Each country performed IHP market study (see right hand box for US IHP Study)

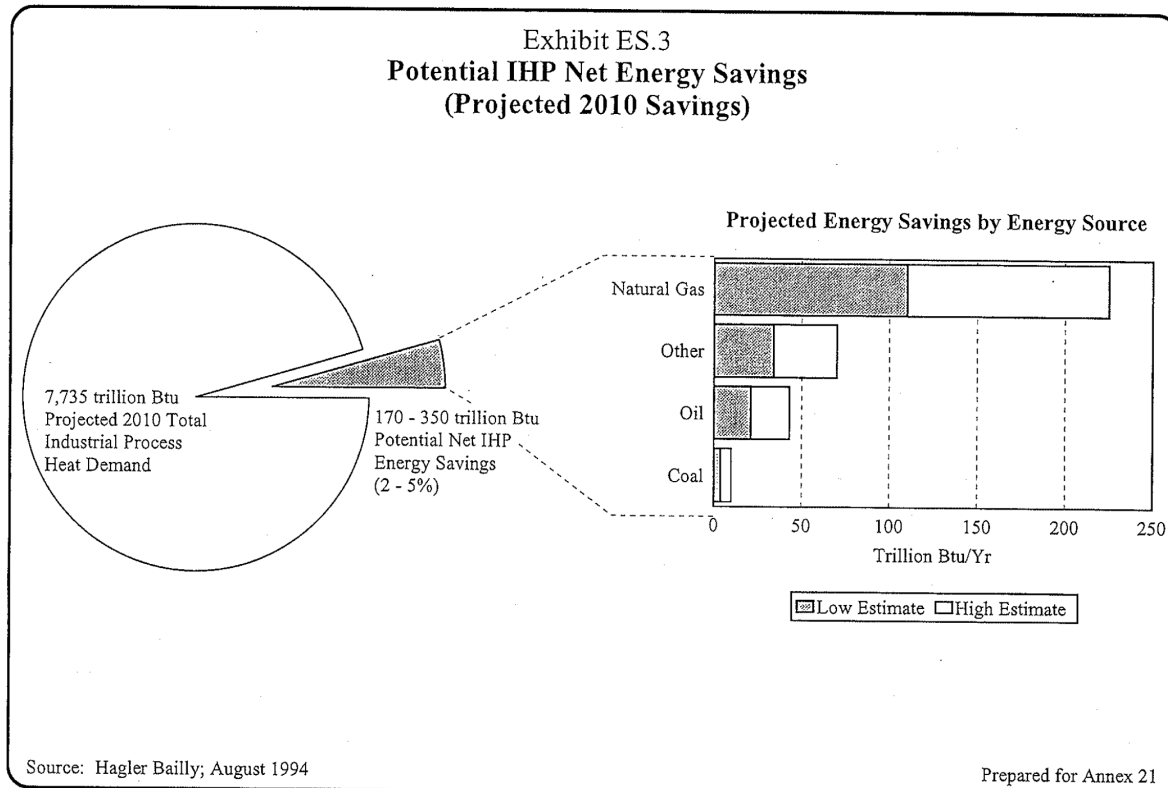
US IHP Market Study

- US study screened 42 processes; 26 found for economic IHP potential
- 8 processes accounted for most (68%) of IHP economic energy savings
 - Corn milling
 - TMP pulp
 - Unbleached kraft linerboard
 - Beet sugar refining
 - Bleached kraft pulp
 - Bleached kraft pulp and paper
 - High fructose corn syrup
 - Synthetic rubber

<https://heatpumpingtechnologies.org/annex21/>



US DOE 1995 Industrial Heat Pump Market Study found 2-5% net process heat savings; 170 - 350 TBtu/yr



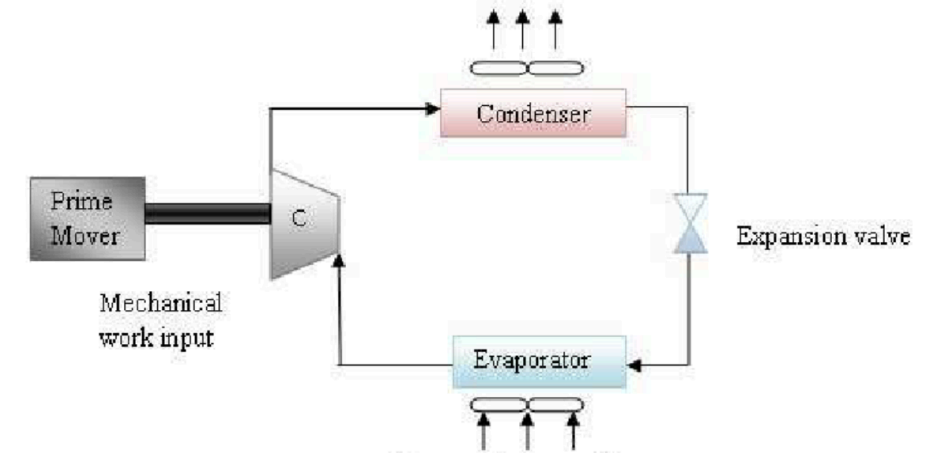
Average Industrial Energy Prices	1995 (2019\$)	2019
Natural Gas (\$/MMBtu)	\$6.56	\$3.85
Electricity Price (cts/kW-hr)	4.28 cts	6.83 cts
Electricity Price (\$/MMBtu)	\$22.16	\$20.00
Electricity/Gas Price Ratio	3.37	5.19

Study 1995
Energy
Prices

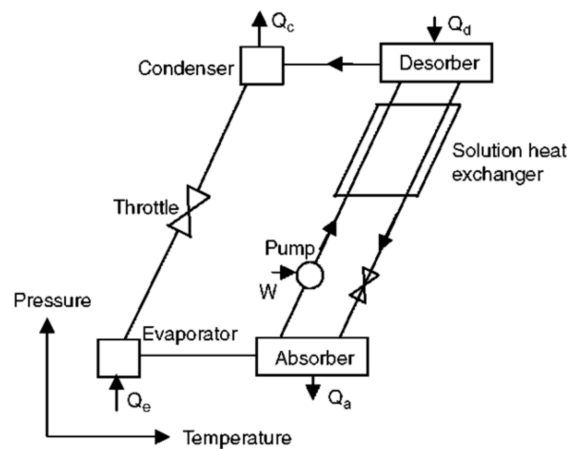
Recent energy
prices are
lower than in
1995

4 High Temperature Heat Pump Types

Cycle Type	High Temperature Heat Pump Type
Closed Cycle	Mechanical vapor compression heat pump
Closed Cycle	Heat activated heat pump: absorption or heat transformer
Open Cycle	Mechanical vapor re-compression (MVR) heat pump
Open Cycle	Thermal vapor re-compression (TVR) or steam ejector heat pump



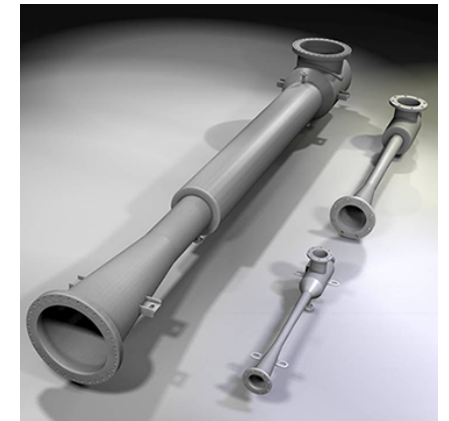
Closed Cycle Mechanical Vapor Compression Heat Pump



Absorption heat pump

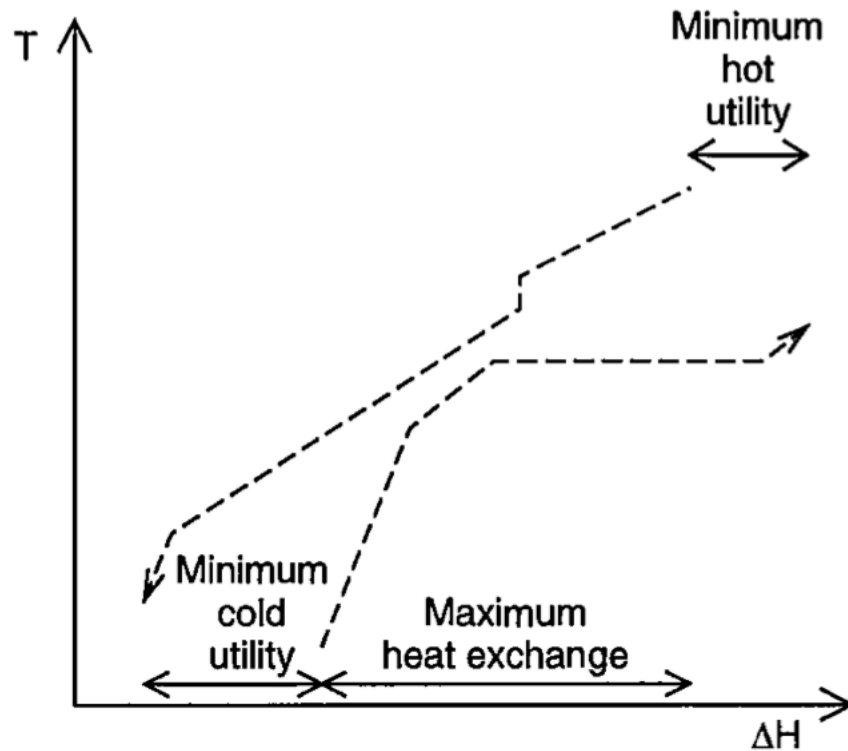


Mechanical vapor recompressor

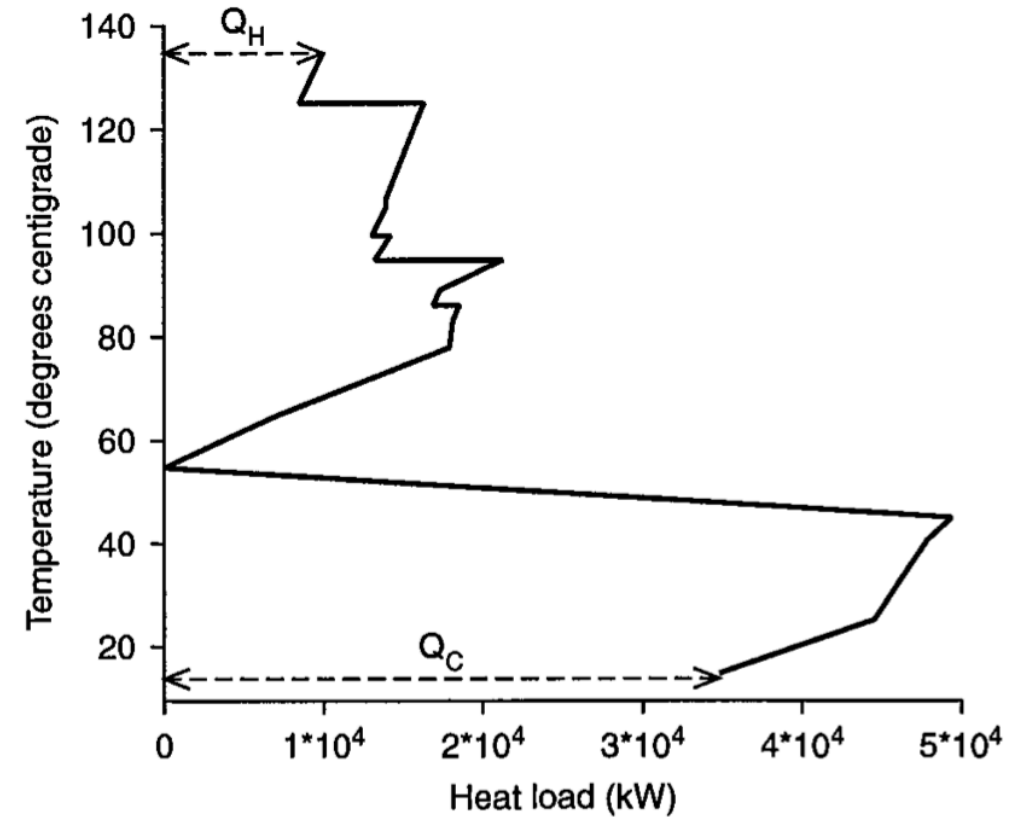


Steam ejector

Heat Integration and Proper Placement of HTHPs with PINCH technology

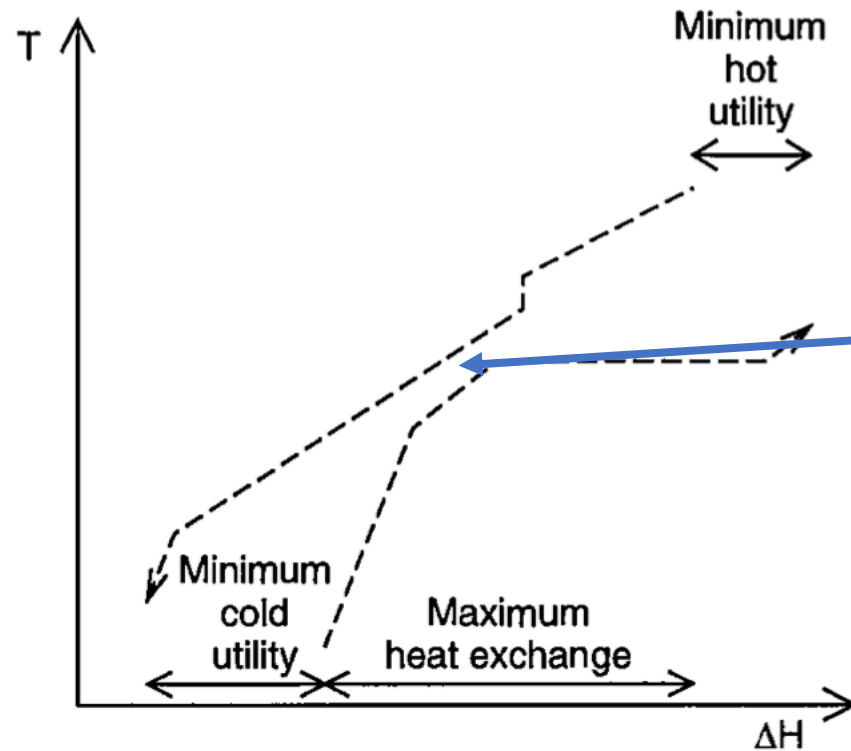


Example Composite curves of heating and cooling streams

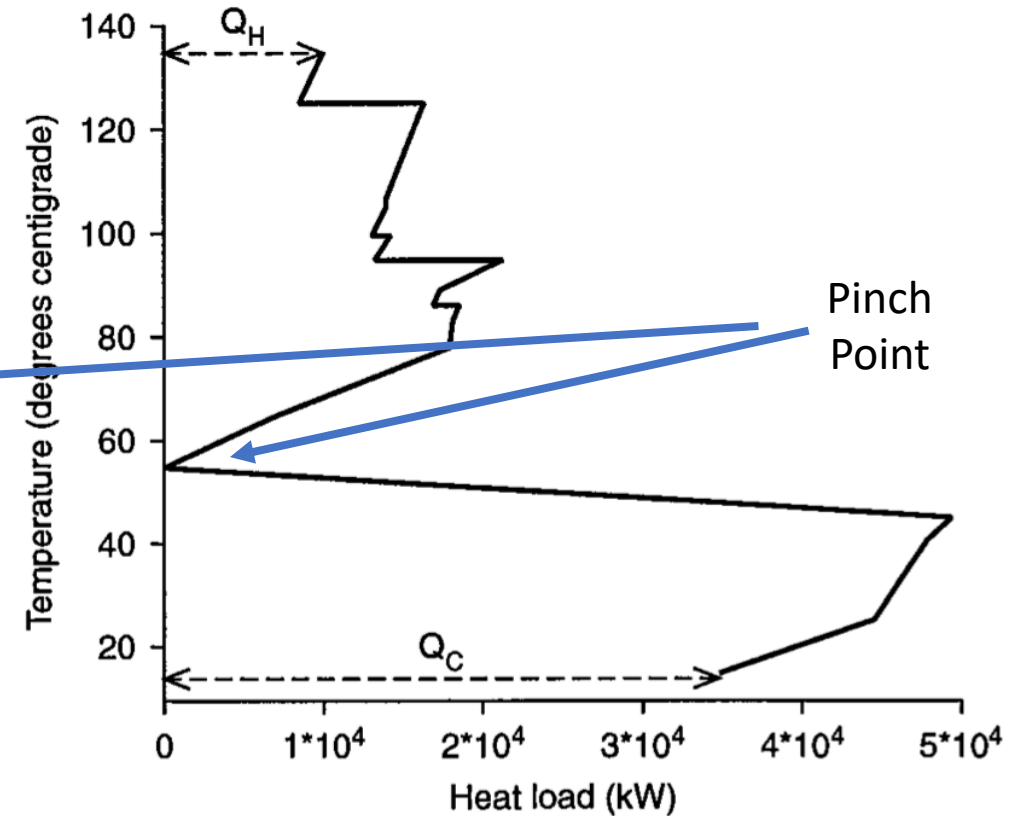


Example Grand Composite Curve

Heat Integration and Proper Placement of HTHPs with PINCH technology

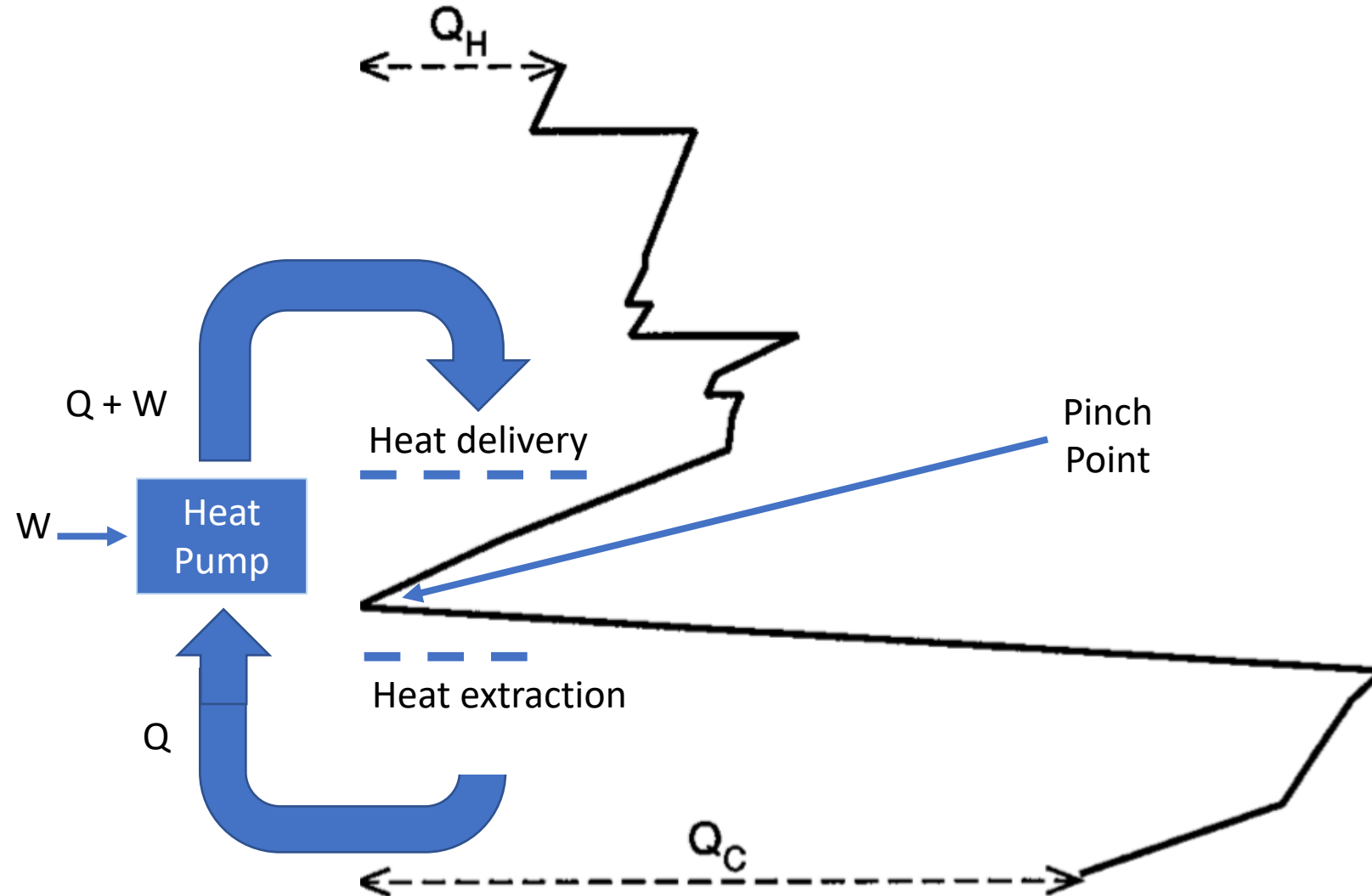


Example Composite curves of heating and cooling streams



Example Grand Composite Curve

Heat Pump should pump
heat around pinch point



Key IHP barriers in the US

Low level of awareness of the technical possibilities and economic feasibility among end users, engineering firms, suppliers, etc.

Lack of knowledge on how to integrate heat pumps into existing industrial processes

Lack of best practice examples to create trust in new type of process heating solution

Most times one-off, tailor-made design and many times need to be integrated to process

Long payback on investment due to low natural gas price and/or high electric to natural gas price ratio

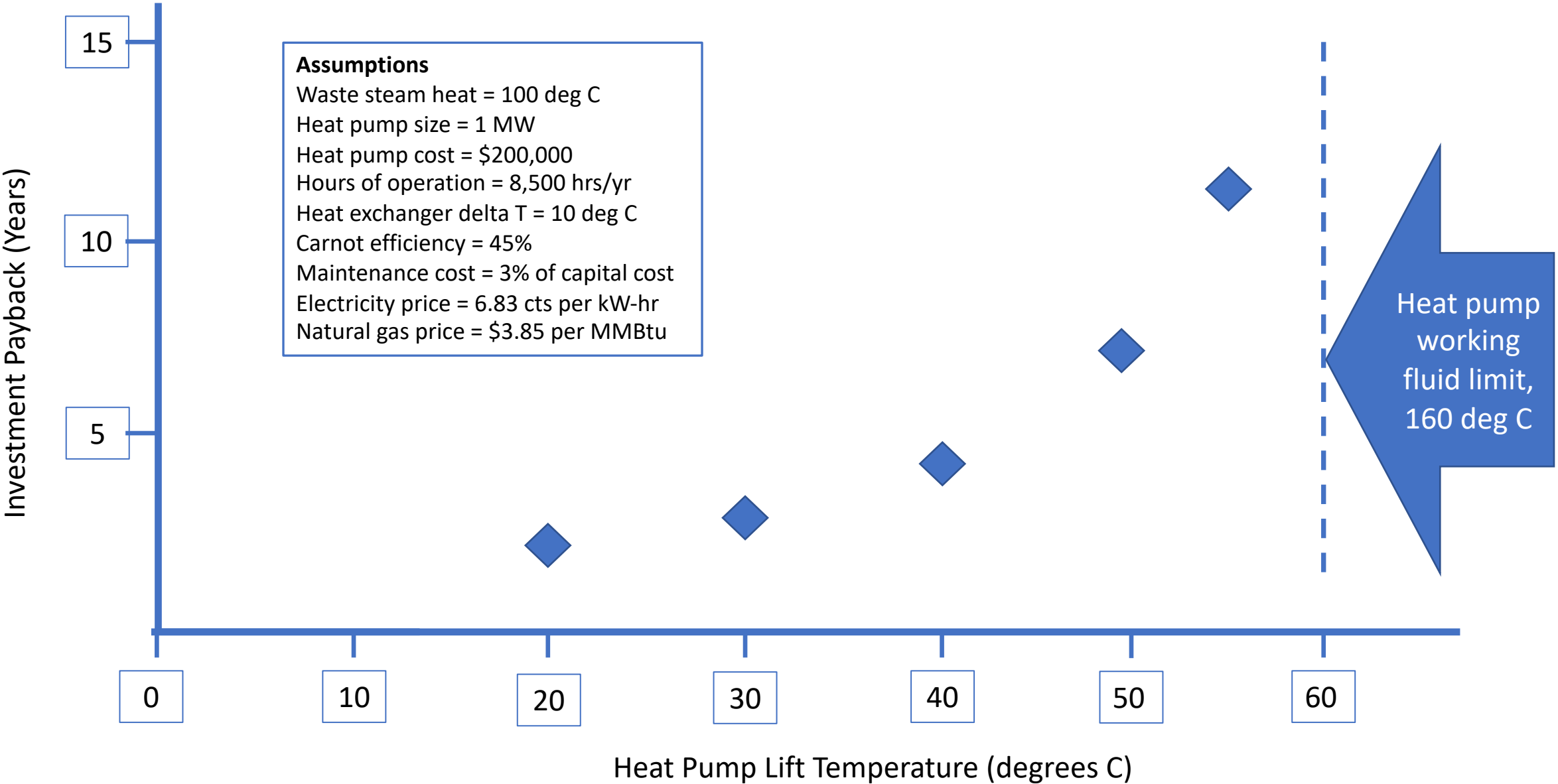
Competing process heating energy efficiency options

Heat storage could be required

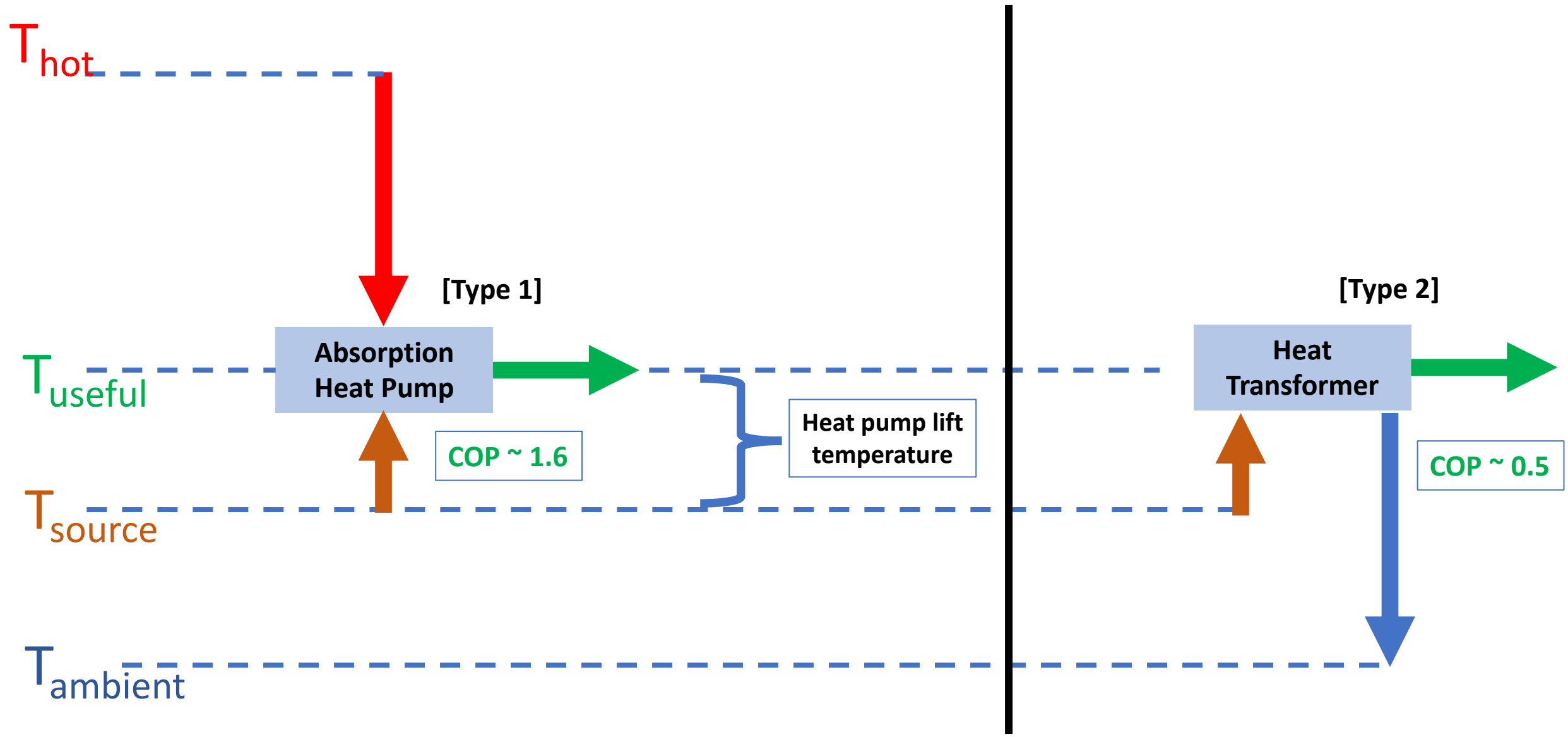
Existing technology limited by heat pump output temperature (~160 deg. C, 320 deg. F)

Limited domestic equipment suppliers – EU, Japan

Mechanical Vapor Compression Heat Pump Payback versus Heat Pump Lift Temperature



What are major technology opportunities that are NOT currently being researched?
Advanced High Temperature Heat-Activated Heat Pumps – Type 1 and 2

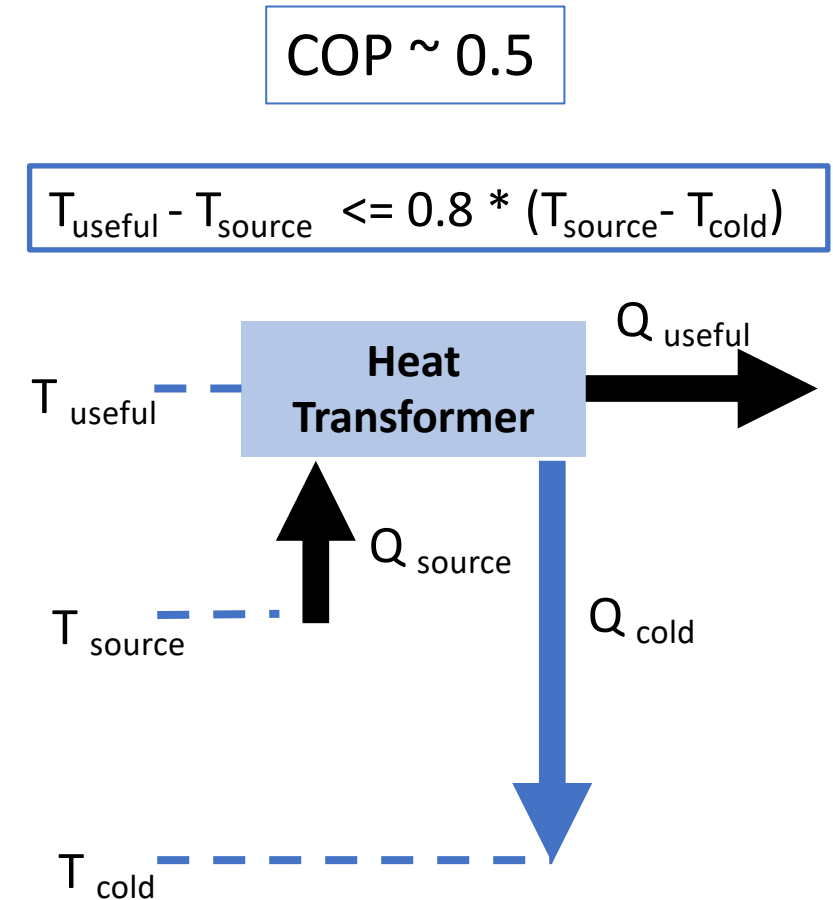


Example Economics for 1 MW Heat Transformer

Q sink = 1 MW @ T sink = 150 deg. C (steam)
Q source = 2 MW @ T source 100 deg. C (steam)
Q cold = 1 MW @ T cold = 30 deg. C
Heat Transformer Cost = \$1.5 Mil (**\$1,500 per kW, pilot unit**)
Annual maintenance cost = 2% of 1.5 Mil = \$30,000 per year
Electricity requirements = 40 kW
Electricity price = 6.83 cts per kW-hr
Operating hours = 8,760 hrs per year
Annual electricity cost = \$24,000 per year
Total operating cost = \$54,000
Natural gas cost = **\$3.85 per MMBtu (avg. US industrial price, 2019)**
Steam cost = \$5.90 per 1000 lb steam
Steam cost savings¹ = \$194,000 per year

Payback = \$1,500,000 / (\$194,000 - \$54,000) = 10.7 yrs

Note 1 – assume 1MW Heat Transformer produces 3750 lbs steam per hr @ 150C and avoids boiler steam and cooling tower costs @ \$5.90 per 1000 lbs steam. Boiler steam costs account for energy cost (natural gas cost and boiler combustion efficiency) and chemical cost needed to treat boiler water.
Private communication Riyaz Papar, January, 2021



Heat Transformer Payback versus Natural Gas Price

Assumptions

Waste steam heat = 100 deg C
Heat pump size = 1 MW
Heat pump delivery temp. = 150 deg C
Heat pump lift temp. = 60 deg C
Hours of operation = 8,760 hrs/yr
Maintenance cost = 2% of capital cost
Electricity consumption = 4% of heat delivery
Electricity price = 6.83 cts per kW-hr

Investment Payback (Years)

10

8

6

4

2

< 5 Year
Payback

Avg. US
industrial
price
(2019)

0

2

4

6

8

10

Natural gas price (\$ per MMBtu)

Heat transformer specific capital cost = \$1,500 / kW

\$1,200 / kW

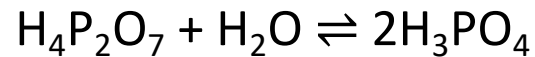
\$900 / kW

Emerging heat-activated heat pump technology

QPinch

Heat-activated heat pump by reversible chemical reaction

phosphoric acid to diphosphoric and water



T_{sink} up to 220 deg. C

Minimal electricity requirements; waste heat-driven

Lift temperature= 40 - 100 deg. C

Multi megawatt demos planned; independent validation needed for:

- Cost and performance
- Reliability and material durability
- Impact on process control



www.qpinch.com

What are the most critical research priorities in HTHPs?

- **Heat-activated heat pumps R&D should focus on:**
 - Developing various Type 1 and 2 cycles and configurations to demonstrate performance and cost
 - Demonstrate heat pump material durability in actual industrial settings and conditions.
 - Demonstrate heat pump operability and reliability in varied industrial processes to prove out economics
 - Prove heat pump working fluids are safe and environmentally benign
- **Technology development R&D targets**
 - Specific capital cost (total installation) < \$1,000 per kW
 - Heat delivery > 200 deg. C and ideally > 250 deg. C
 - Lift temperature up to 100 deg. C

Conclusions

There's reason to be optimistic about High Temperature Heat Pumps

- 1. New perspective by industry:** Companies that are serious about decarbonizing their energy footprints will consider HTHPs if they yield significant (>5 – 10%) energy savings and decarbonization at a reasonable payback, e.g., less than 5 years.
- 2. R&D justified to build domestic High Temperature Heat Pump industry:** Advanced heat-activated heat pumps could be a game-changer to greatly expand the number of economic opportunities in the US process industries - - even with only modest increases in natural gas prices. Cost-shared R&D in the US should help build the domestic supplier base for high temperature heat pumps.
- 3. Technology development is not enough:** Further technology development is needed and justified but needs to be coupled with effective energy policy and/or incentives to motivate all participants in HTHP market – end users, vendors, engineering firms and energy efficiency program administrators/utilities.

Background Slides

Mechanical vapor compression heat pumps; reference Cordin Arpagaus, 2020

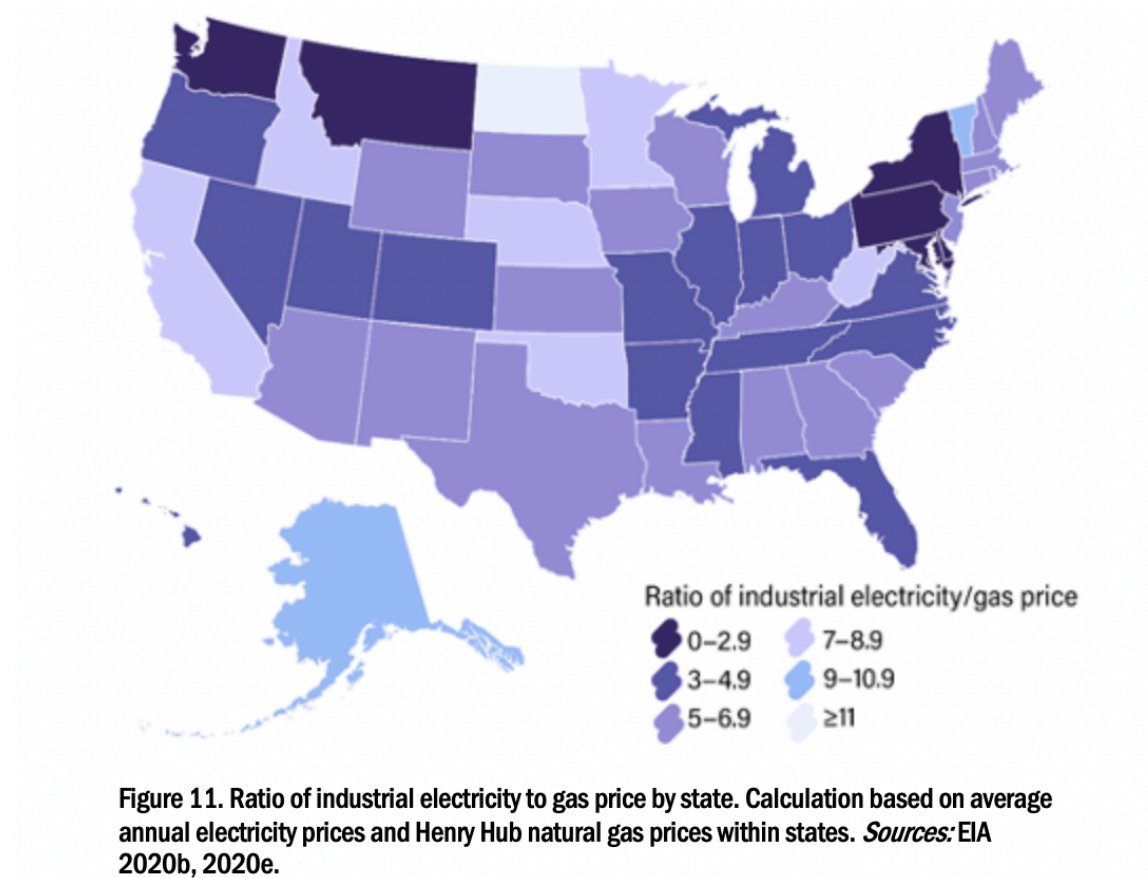
Supplier update – market overview



Selection of industrial heat pumps with heat supply temperature $\geq 90\text{ }^{\circ}\text{C}$

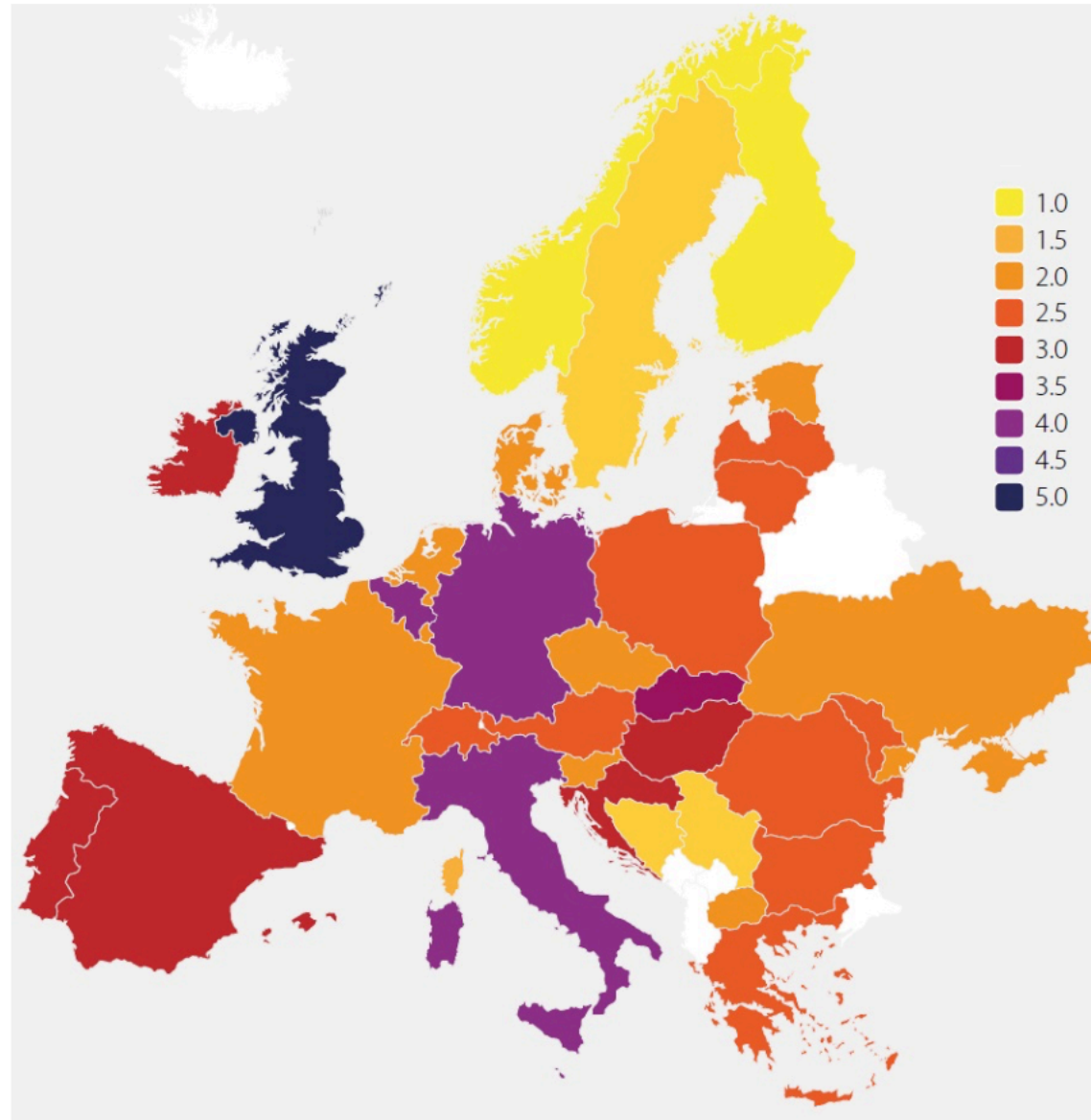
Manufacturer	Country	Product	Refrigerant	Max. T _{Supply}	Heating capacity	Compressor type
Kobe Steel (Kobelco steam grow heat pump)		SGH 165	R134a/R245fa	165 °C	70 – 660 kW	Double screw
		SGH 120	R245fa	120 °C	70 – 370 kW	
		HEM-HR90,-90A	R134a/R245fa	90 °C	70 – 230 kW	
Viking Heating Engines AS		HeatBooster	R1336mzz(Z)	160 °C	28 – 188 kW	Piston
		HeatBooster S4	R245fa	130 °C	92 – 172 kW	(4 parallel)
Ochsner		IWWDSS R2R3b	R134a/ÖKO1	130 °C	170 – 750 kW	Screw (TWIN unit upto 1,5 MW)
		IWWDSS ER3b	ÖKO1 (R245fa)	130 °C	120 – 400 kW	
		IWWHS ER3b	ÖKO1 (R245fa or R1233zd)	95°C	60 – 640 kW	
Frigopol (& AIT)		HighButane 2.0	R600	130 °C	50 kW	Piston
Hybrid Energy		Hybrid Heat Pump	R717 (NH ₃)	120 °C	0.25 – 2.5 MW	Piston
Mayekawa		Eco Sirocco	R744 (CO ₂)	120 °C	65 – 90 kW	Screw
		Eco Cute Unimo	R744 (CO ₂)	90 °C	45 – 110 kW	
Combitherm		HWW 245fa	R245fa	120 °C	62 – 252 kW	Piston
		HWW R1234ze	R1234ze(E)	95 °C	85 – 1301 kW	
ENGIE (ex-Dürr thermea)		Thermeco ₂ HHR	R744 (CO ₂)	110 °C	45 – 1'200 kW	Piston (up to 6 parallel)
Oilon		ChillHeat	R134a	100 °C	30 – 1'000 kW	Piston
		P60 bis P450	R1234ze(E)			(up to 6 parallel)
Friotherm		Unitop 22	R1234ze(E)	95 °C	0.6 – 3.6 MW	Turbo (two-stage)
		Unitop 50	R134a	90 °C	9 – 20 MW	
Star Refrigeration		Neatpump	R717 (NH ₃)	90 °C	0.35 – 15 MW	Screw (Vilter VSSH 76 bar)
GEA Refrigeration		GEA Grasso FX P 63 bar	R717 (NH ₃)	90 °C	2 – 4.5 MW	Double screw (63 bar)
Johnson Controls		HeatPAC HPX	R717 (NH ₃)	90 °C	326 – 1'324 kW	Piston (60 bar)
		HeatPAC Screw	R717 (NH ₃)	90 °C	230 – 1'315 kW	Screw
		Titan OM	R134a	90 °C	5 – 20 MW	Turbo
Mitsubishi		ETW-L	R134a	90 °C	340 – 600 kW	Turbo (two-stage)
Viessmann		Vitocal 350-HT Pro	R1234ze(E)	90 °C	148 – 390 kW	Piston (2 to 3 in parallel)

Ratio of Industrial electricity/gas Price



Market challenges

Electricity to gas price ratio



For small scale industrial
end-users with
2 GWh/a to 20 GWh/a electricity
3 GWh/a to 28 GWh/a gas

IHP types: Pros and Cons. What are the pros and cons of various HTHP types?

Type	Prime Mover	Pros	Cons	Typical COP
Closed cycle compression	Electricity (Motor) or Fuel (Heat Engine)	<ul style="list-style-type: none">- Good COP for moderate lift temperature- Multiple vendors- Electricity only on site	<ul style="list-style-type: none">- Requires low electric-fuel price ratio- Limited supply temperature to ~320F supply	3 to 10
Heat-activated (Type 1)	Fuel (Process Heat or Steam)	<ul style="list-style-type: none">- Uses lower cost fuel as driver- Minimal moving parts- Higher supply temperature ~400F	<ul style="list-style-type: none">- High CapEx- Limited vendors- Emerging technology	1.6
Heat-activated (Type 2)	Waste heat	<ul style="list-style-type: none">- Uses free waste heat as driver- Minimal moving parts- Higher supply temperature ~400F	<ul style="list-style-type: none">- High CapEx- Limited vendors- Emerging technology- Requires cold sink T_{Δ}	0.5
MVR	Electricity (Motor) or Fuel (Heat Engine)	<ul style="list-style-type: none">- Good COP for moderate lift temperature- Electricity only on site	<ul style="list-style-type: none">- Requires low electric-fuel price ratio- High speed compressor	3 to 10
TVR	Steam	<ul style="list-style-type: none">- Low CapEx- Simple and low maintenance	<ul style="list-style-type: none">- Low energy efficiency	2.0